



Hydrogen from biomass via thermo-chemical route – Status of development and perspectives

Univ. Prof. DI Dr. Hermann Hofbauer Vienna University of Technology Bioenergy2020+ GmbH







Content

- Process chains for hydrogen production
 - Methane to hydrogen
 - Biomass to hydrogen
 - Chemical reactions and maximal yields
- Polygeneration with hydrogen production
 - Definition
 - CHP and pilot plant Oberwart
 - Polygeneration process chains
 - Experimental results
- hydrogen-electric vision
- Conclusions

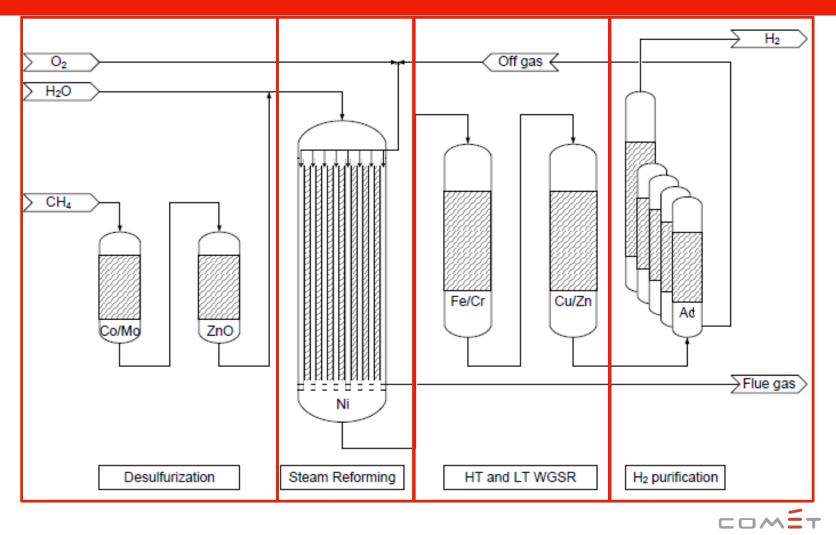








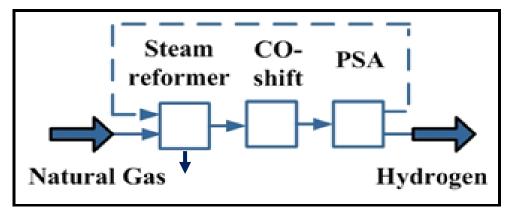
Conventional process chain: Natural gas to hydrogen







Conventional process chain: Natural gas to hydrogen



Plant In	put *		Plant Output *					
Natural Gas	Nm ³ /h	3 822	Hydrogen	Nm³/h	10 040			
Natural Gas (lhv)	MJ/Nm ³	36.91	Hydrogen (lhv)	MJ/Nm ³	10.79			
Natural Gas (chem. en.)	MW	39.2	Hydrogen (chem. ener.)	MW	30			
Electricity	MW	0.3	Steam (48 bar _{abs})	t/h	12.4			
Steam (26 bar _{abs})	t/h	8.7						
*Plant size [4] reduced to 30	MW H ₂ Outp	put (~16%)	H ₂ -Efficiency: 76 %					

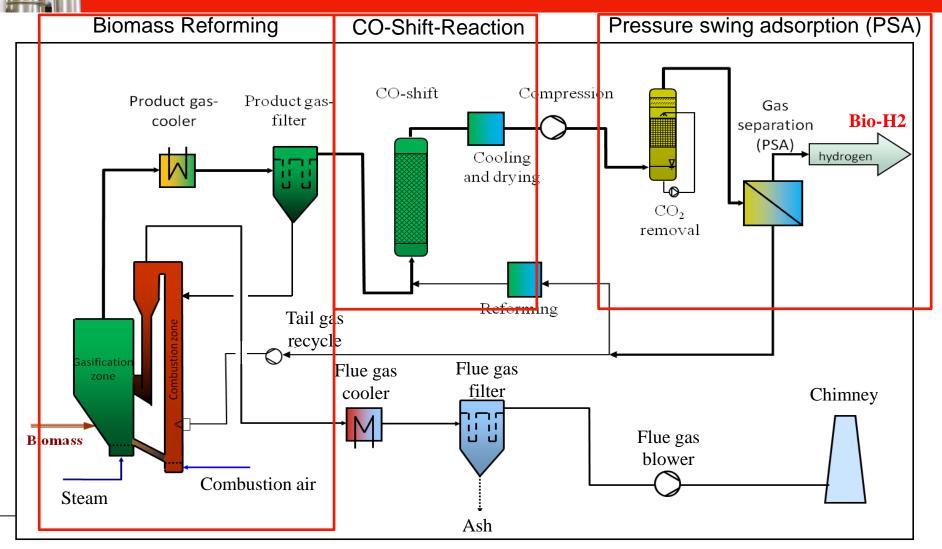






Process chain: Biomass to hydrogen (1)

Project: "BioH₂-4Industries"





bioenergy2020+

Process chain: Biomass to hydrogen (2)

Project: "BioH₂-4Industries" - Results from simulation

and a	Plant input				E4					
	Biomass (wood chips)	kg/h	18 760	мw	 76 %	fficienc	у. 60 %			
	Biomass (water content)	wt%	40	60 -	10 /0		00 /0			
	Biomass (lhv)	MJ/kg	9.59					N	latural G	as
Ω	Biomass (chem. energy)	MW	50				6.6	E B	iomass	
	Electricity *	MW	6.58					<mark>=</mark> E	lectricity	1
	RME	kg/h	100	40 -				E H	ydrogen	n
	Air	Nm ³ /h	57 400		0.3					
	Water	kg/h	3 327							
	* excl. Electricity for cooling	cooling and CO ₂ separation								
	Plant output									
	Hydrogen	Nm³/h	10 040	20 -	39.1		50		30	
	Hydrogen (lhv)	MJ/ Nm ³	10.79							
	Hydrogen (chem. energy)	MW	30							
	Pure CO_2 (from separ.)	Nm³/h	5 923							
	District heating	MW	8.9							
	Ash	kg/h	1 036		0 H2 from Natural Gas H2 from Biomass Plan					
	Flue gas	Nm³/h	61 800		s Pi	Plant Output				
					Plant Input		ant Input			







Production of hydrogen Steam reforming

General

```
CH_nO_m + (1-m).H_2O = CO + (1+n/2-m).H_2
```

```
Methane (n=4, m=0)
```

 $CH_4 + H_2O \underbrace{CO} 3.H_2$

Biomass (n=1,44, m=0,66)

$$CH_{1,44}O_{0,66} + 0,34.H_2O = CO + 1,06.H_2$$

Reaction conditions:

800-900 °C

Catalysts: Ni, Ca, Fe







Production of hydrogen Water-Gas-Shift-Reaction (WGSR)

Water-Gas-Shift-Reaction (WGSR)

 $CO + H_2O = CO_2 + H_2$

 $CO + 3.H_2 + H_2O = CO_2 - 4.H_2$

Maximum Yields

500 g_{H2} / kg_{nat.gas} ~ 10 kg_{H2} / GJ

Biomass:

Methane:

$$CO + 1,06.H_2 + H_2O = CO_2 + 2,06.H_2$$

172 g_{H2} / kg_{wood} ~ 10 kg_{H2} / GJ

WGSR conditions:

350-450 °C

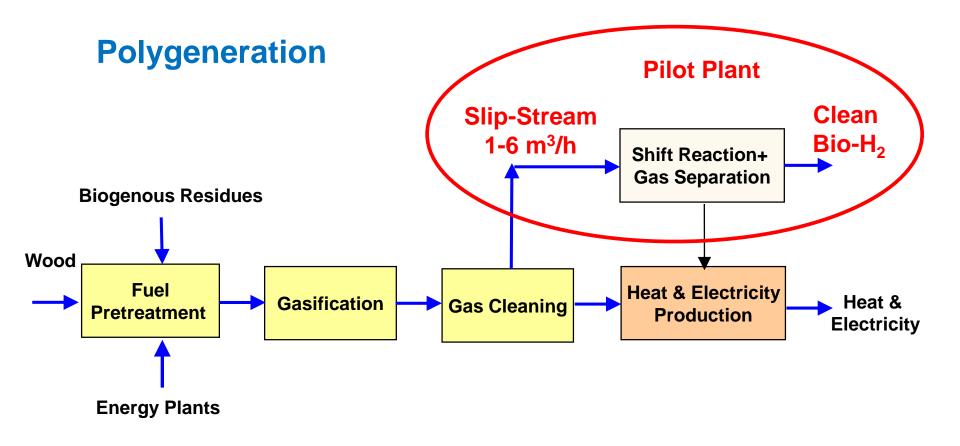
Catalysts: Fe, Cr, Co, Mo, Sn





bioenergy2020+

Polygeneration process chain Biomass to hydrogen and other products

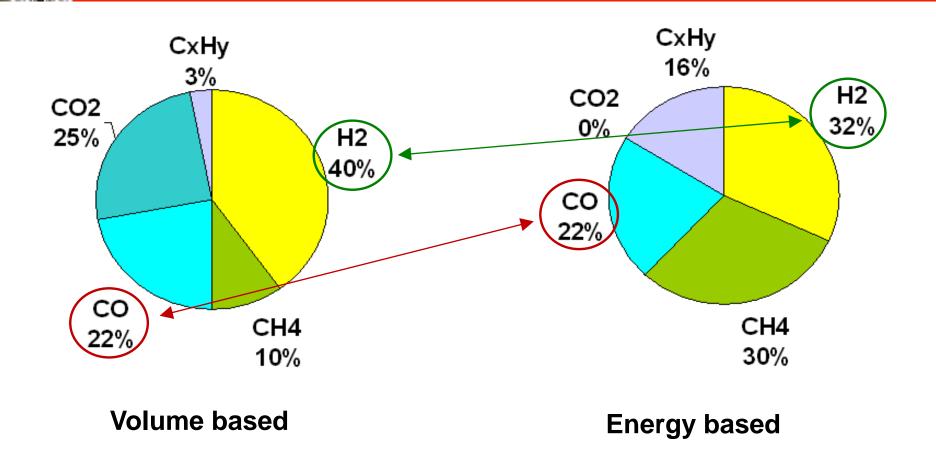








Product gas from biomass steam reforming





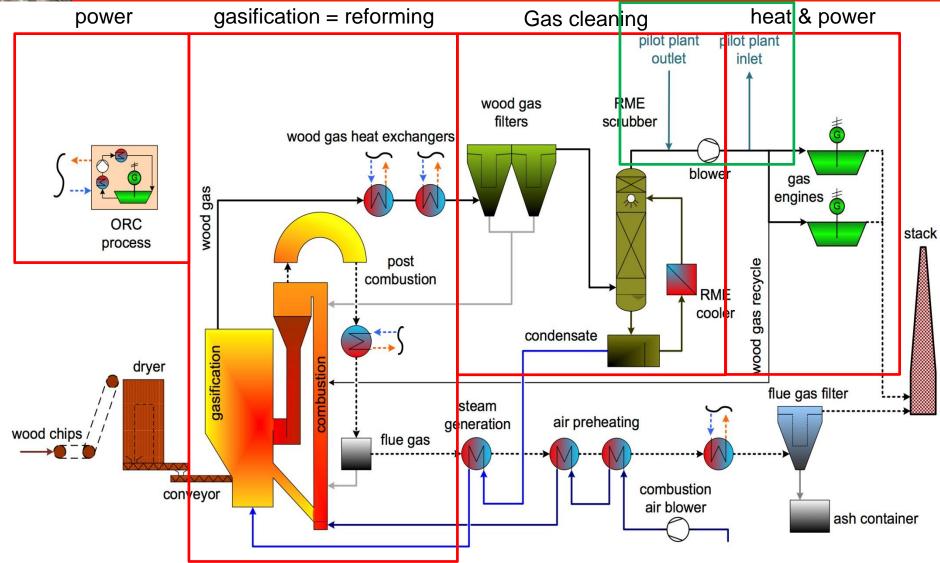
Gasification plant Oberwart 8 MW fuel input 2000 kg/h wood chips 2000 m³/h product gas 30 % electrical efficiency 30.000 operation hours

7



TECHNISCHE UNIVERSITÄT WIEN Vienna University of Technology

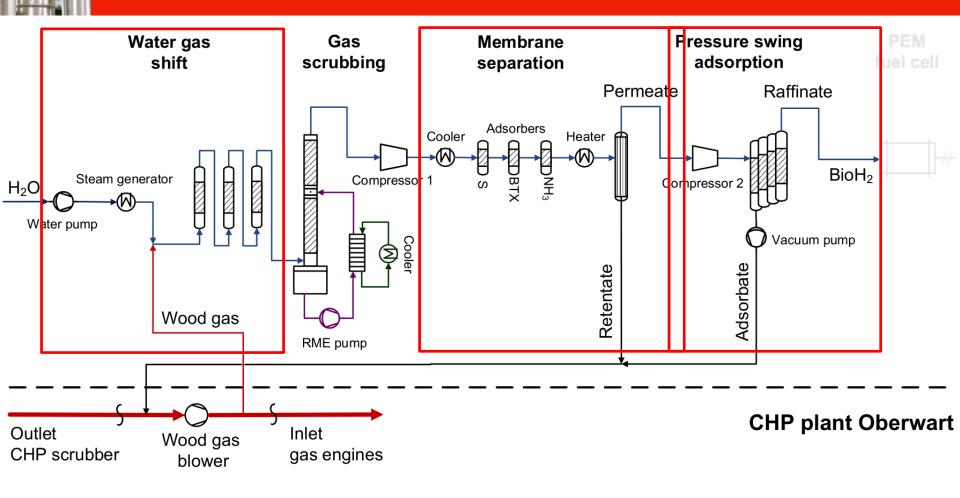








Polygeneration Full process chain for hydrogen production









Container with pilot plant at CHP Oberwart







Membran

View into research container (1) left hand side

TUTVT

Pressure Swing Adsorption

bioenergy2020

PEM Fuel Cell



bioenergy2020+

View into research container (2) right hand side

Water Gas Shift Reaction

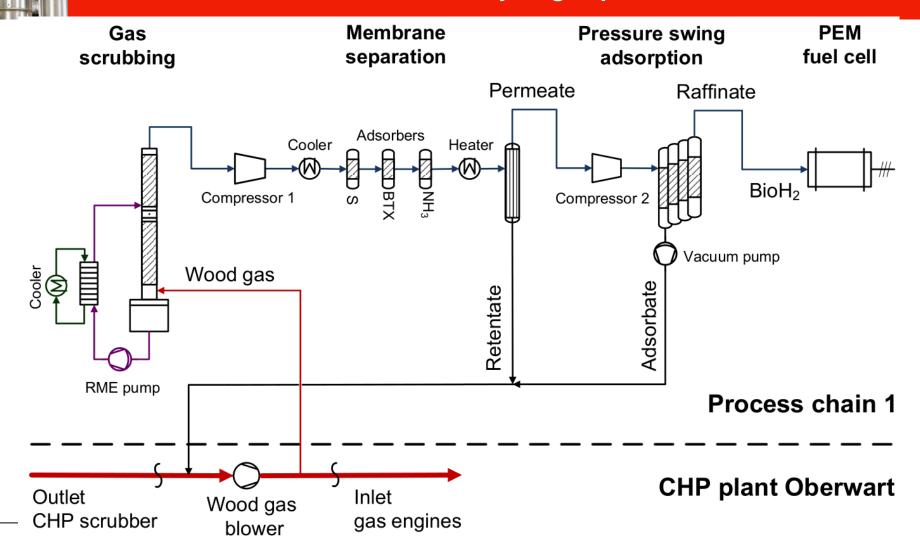


In the state of th





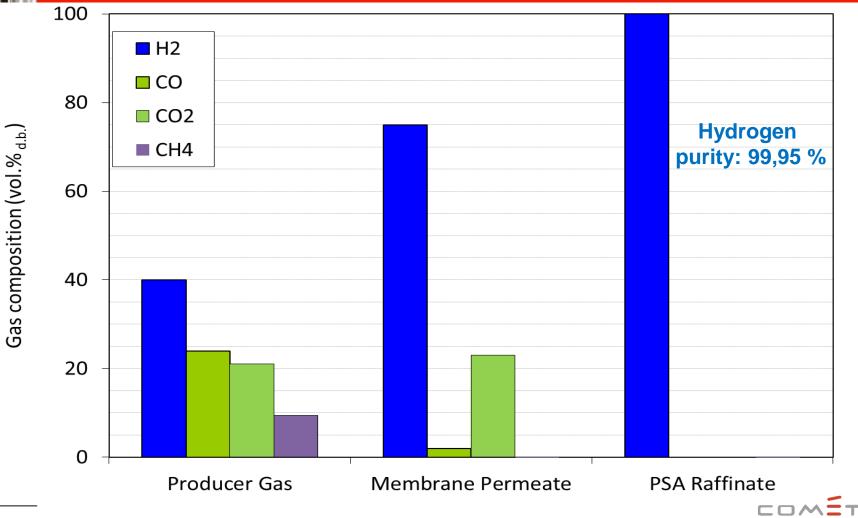
Polygeneration Process chain 1 for hydrogen production







Main gas components along the process chain 1





Data for PEM-fuel cell

- Type: PEM FC "Mobixane"
- Nominal load: 2500W
- Minimal load: 500W
- Electrical efficiency: about 50 %

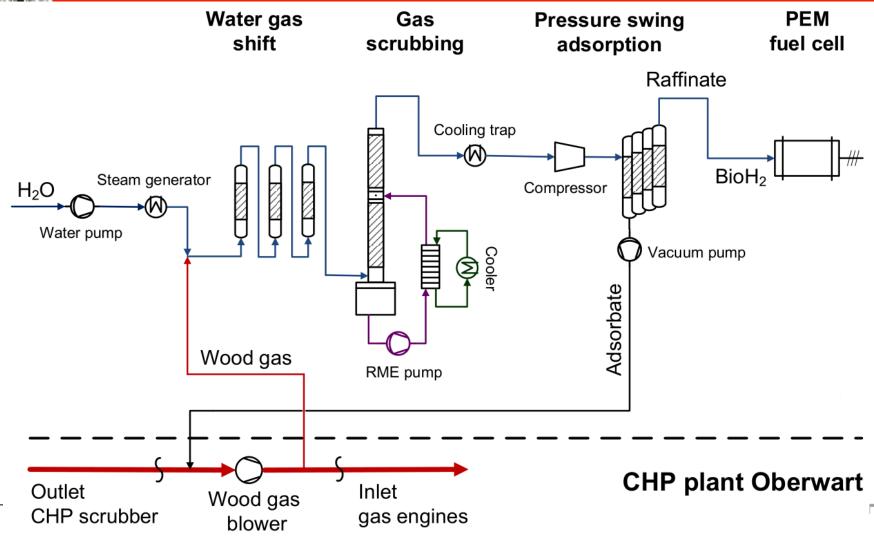








Polygeneration Process chain 2 for hydrogen production

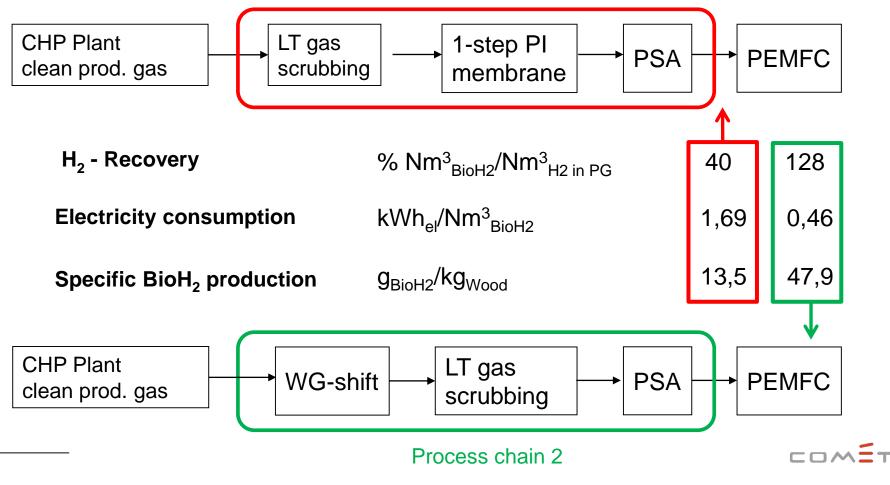






Comparison of performance data of process chain 1 and 2

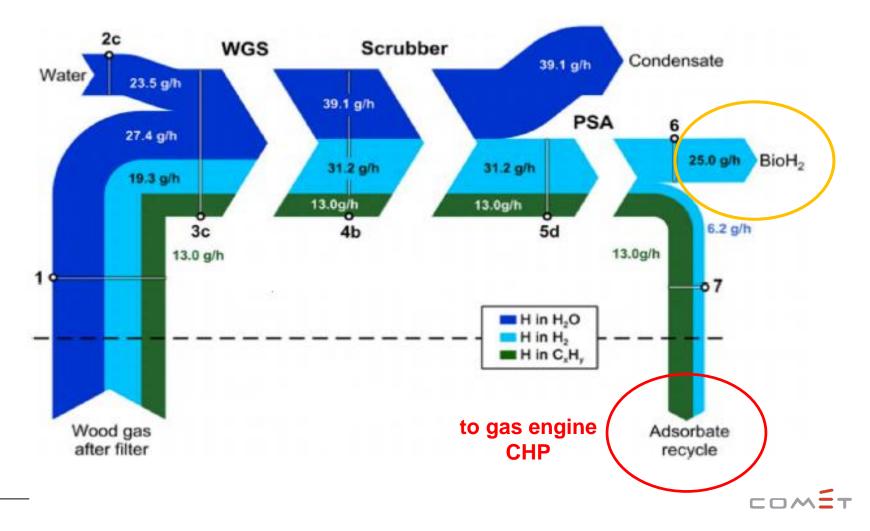




bioenergy2020+



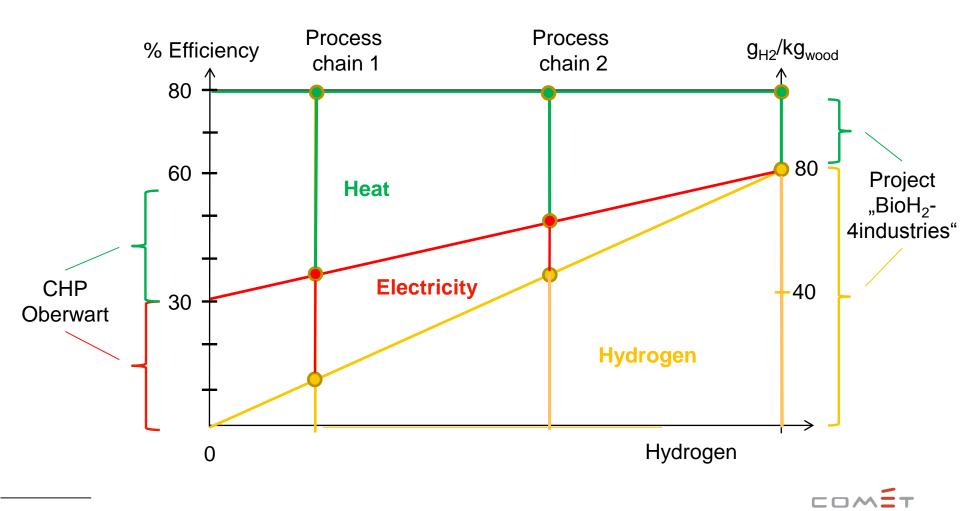
Hydrogen mass flows of process chain 2







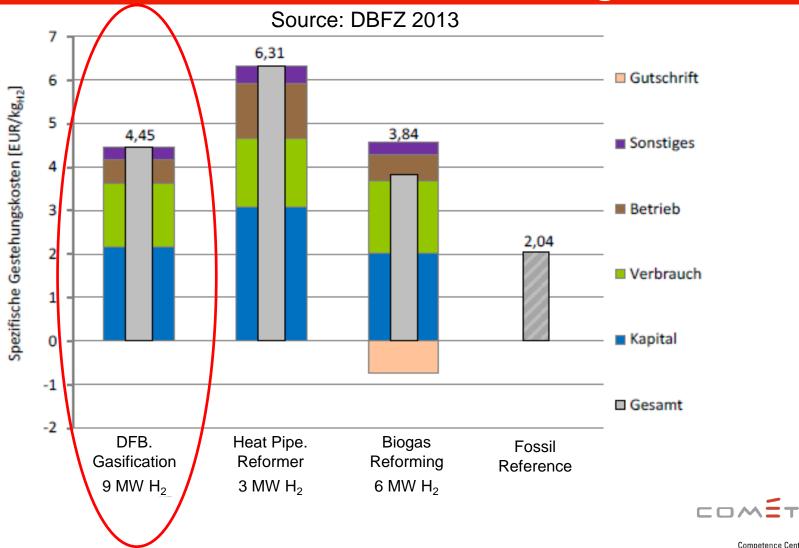
Polygeneration – flexibility & potential

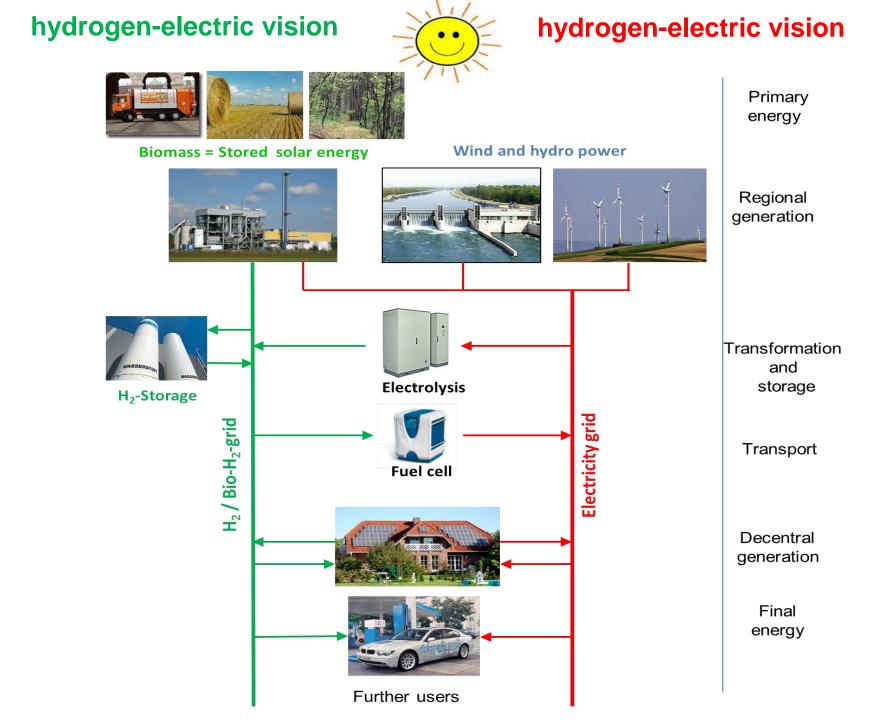




bioenergy2020+

Economic analysis of hydrogen production based on steam reforming







Thank you for your kind attention !





VIENNA UNIVERSITY OF TECHNOLOGY Institute of Chemical Engineering



bioenergy2020+

BIOMASS-TO-HYDROGEN

Univ. Prof. Dr. Hermann Hofbauer Vienna University of Technology, Institute of Chemical Engineering A-1060 Getreidemarkt 9/166

