

# A3-FALCON: Advanced FC Analysis, Diagnostics and its Application

## CFD Simulation

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## Introduction

- Working principle of a PEM fuel cell
- Why detailed electrochemical 3D simulation?

## Overview of AVL FIRE Fuel Cell Module

### Simulation of AC64-5 stack by IE and comparison to experimental data

- Healthy (new) stack
- Degraded (used) stack

## Conclusions and outlook



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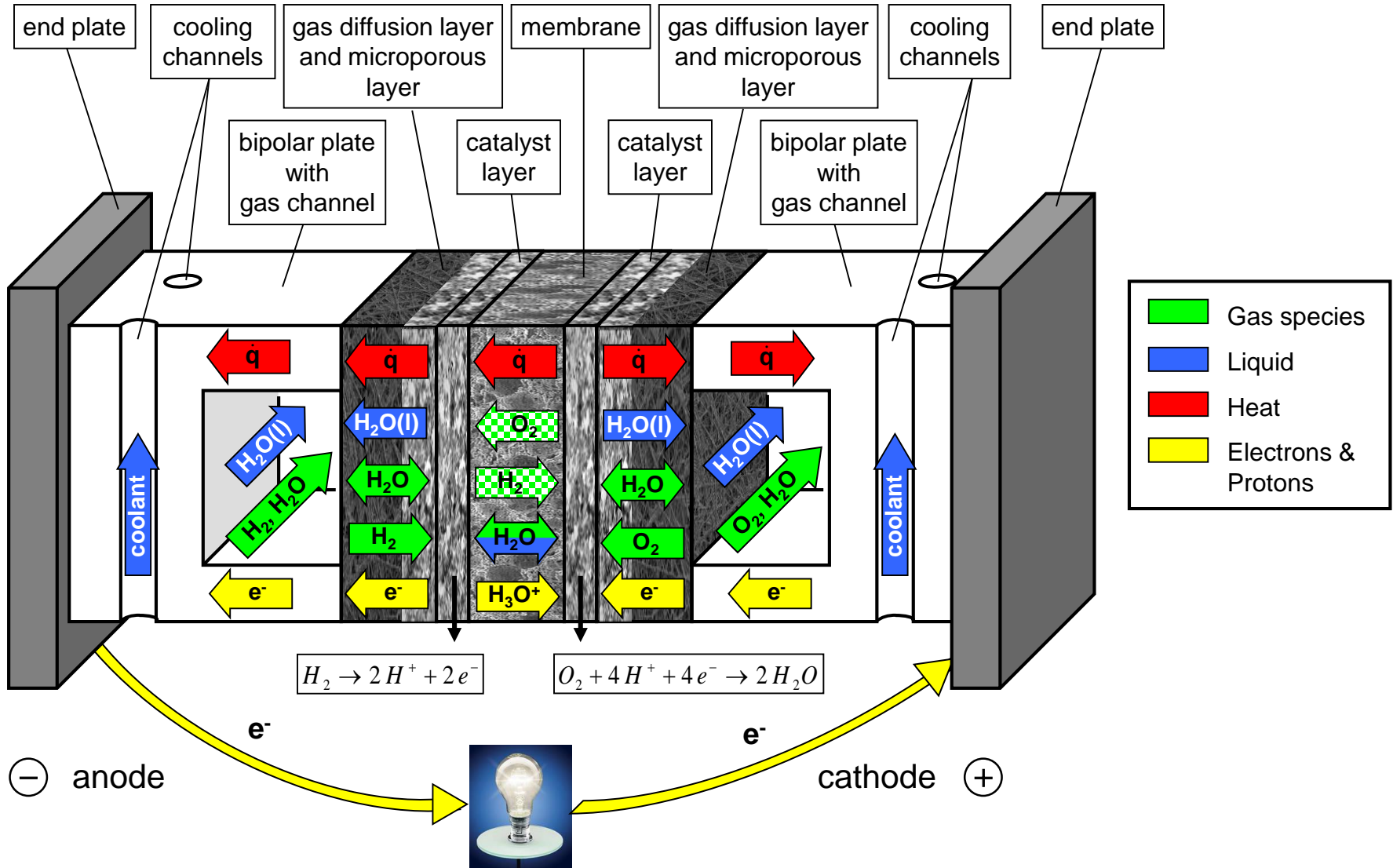
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# Introduction – Working principle of a PEM fuel cell





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## Identification of critical locations

- E.g. hot spots, local water flooding, local fuel starvation
- ⇒ Optimization of geometry, e.g. layer thicknesses or channel dimensions and structure

## Identification of critical operating conditions

- E.g. performance decrease if inlet gases too dry (membrane dries out) but also if they are too humid (water flooding)
- ⇒ Optimization of operating conditions, e.g. temperature, pressure, mass flow rates, relative humidity

## Investigation of material parameters

- E.g. effect of the electrode's pore size on performance
- ⇒ Finding optimum compromise between material costs and performance

## Conclusions to cell degradation and lifetime

## Exploitation of 3D results for further analysis

- E.g. 3D temperature field calculated with FIRE used as input for stress analysis



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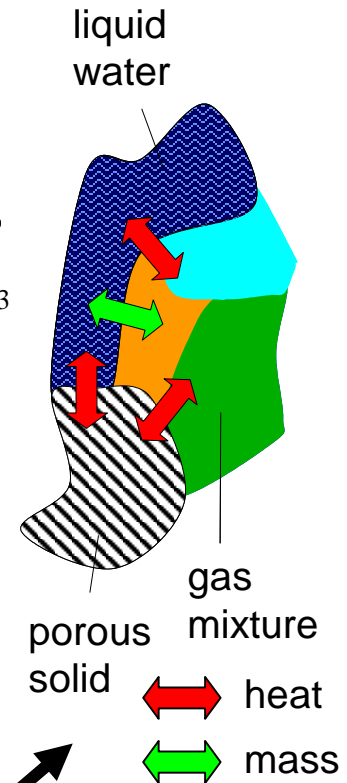
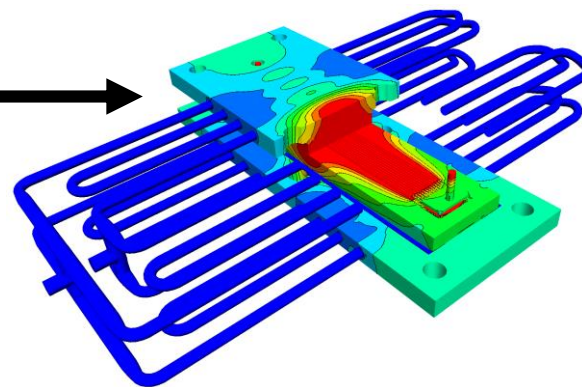
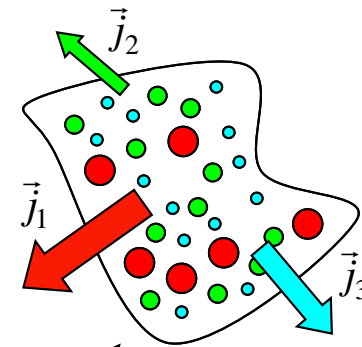
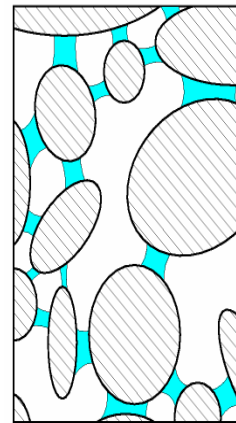
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3D distributions of the following physical quantities are calculated

- Electronic potential in all electron conducting solids
- Ionic potential in all ion conducting solids / liquids (electrolyte)
- Velocity, pressure, and volume fraction of all liquids / gases
- Species mass fractions in all multicomponent gases
- Temperature in all thermally conducting solids / liquids / gases
- Water concentration in electrolyte
- Parasitic gas species concentrations in electrolyte



Underlying transport equations coupled via mass, heat, and charge source terms



## Degradation model developed in A3-FALCON by TU Graz

- Degradation of membrane, catalyst layer and GDL based on empirical and semi-empirical relations
- Following material and geometry parameters are modified dependent on temperature, pressure, humidity, voltage and operating time
  - Membrane thickness
  - Ionic conductivity
  - Sulfonic acid group concentration
  - Gas species diffusion coefficients in membrane
  - GDL thickness
  - Contact angle in GDL
  - Exchange current density in cathode catalyst layer
- Parameters adapted automatically during simulation; only user input: operating time & membrane type



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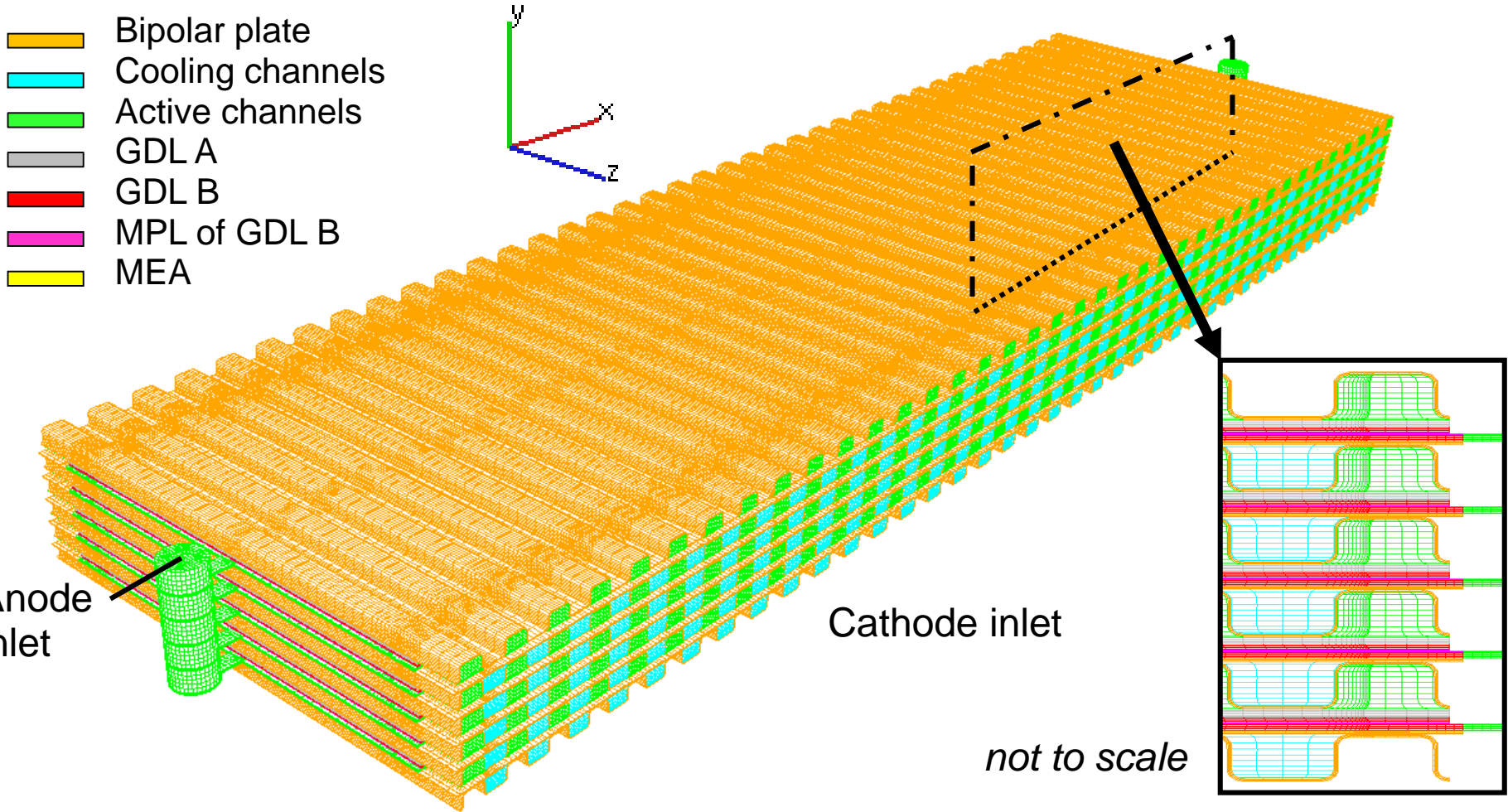
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# Simulation of AC64-5 stack – healthy (new) stack

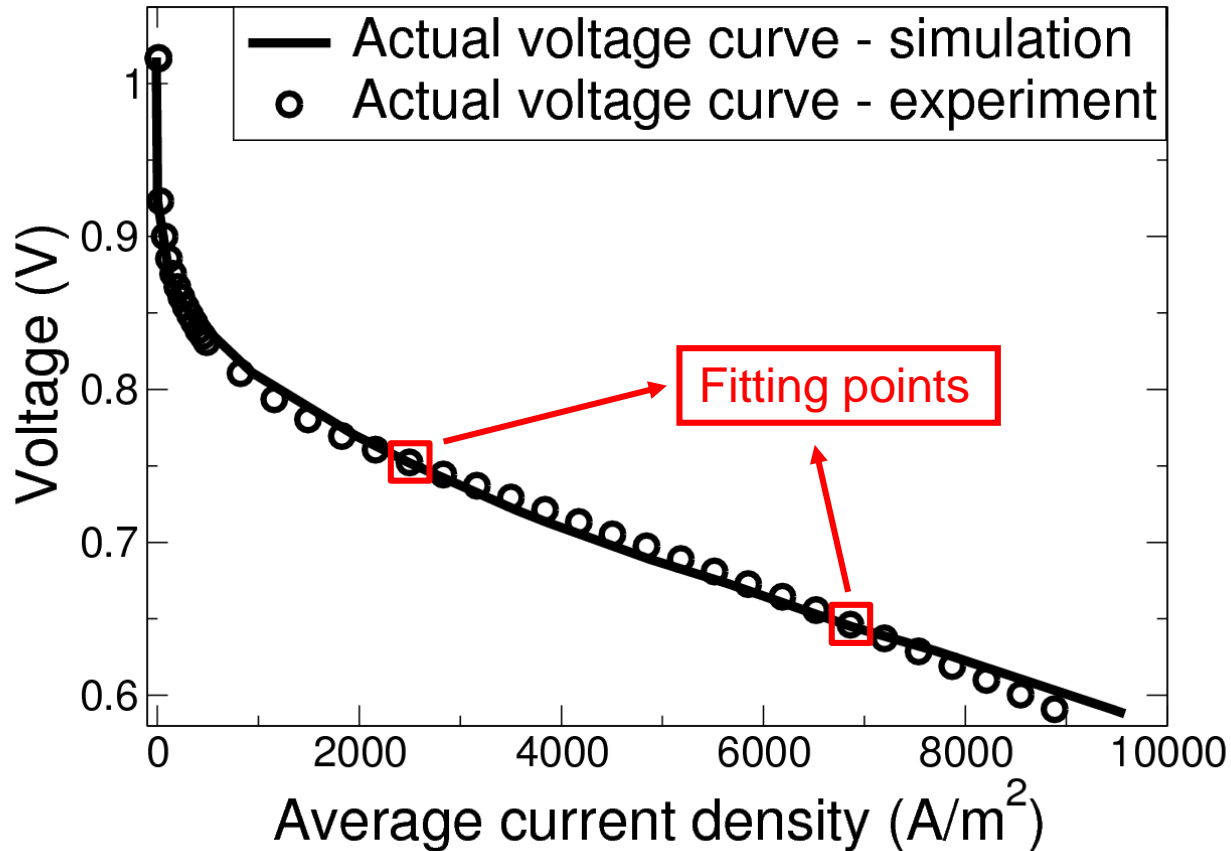


Computational mesh of AC64-5 stack, 9.114.628 cells





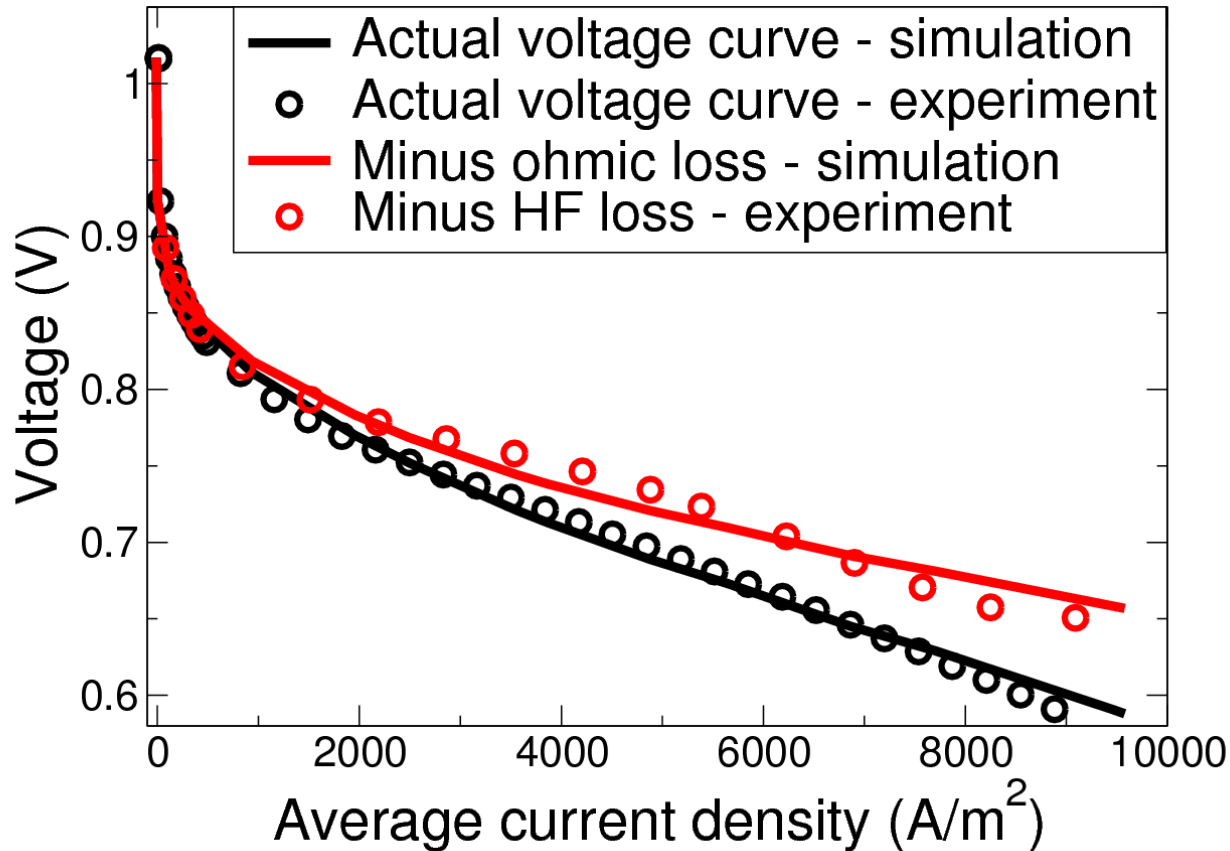
VI curve (simulation: single cell, measurement: 6-cell stack)



- Excellent fit, current density in low voltage range slightly overestimated



VI curve with ohmic potential loss



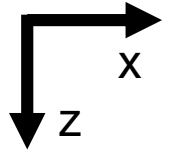
- Good agreement also in ohmic overpotential



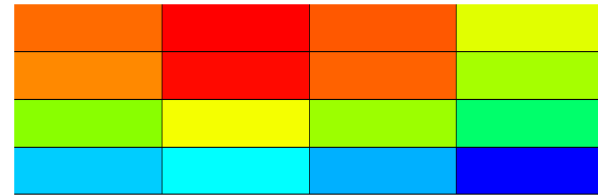
# Simulation of AC64-5 stack – healthy (new) stack



Current density (left) and temperature (right) in experiment and simulation



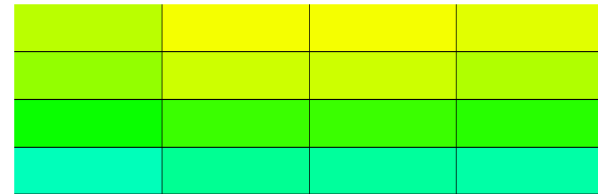
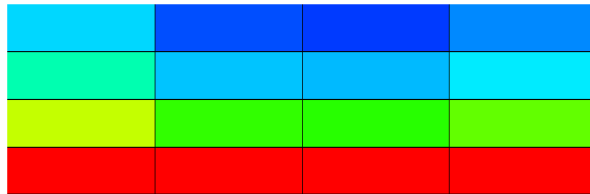
Experiment:



*not to scale*

*not to scale*

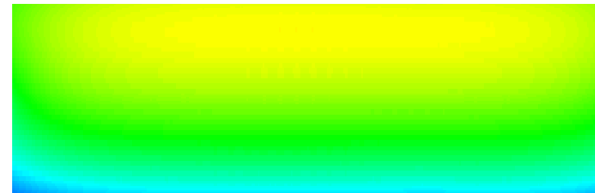
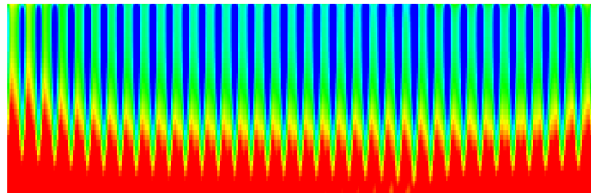
Simulation (resolution of measurement plate):



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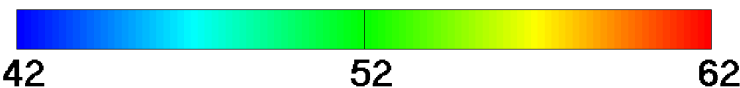
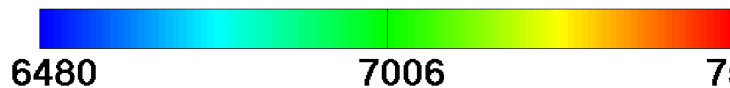
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Simulation (resolution of computational mesh):



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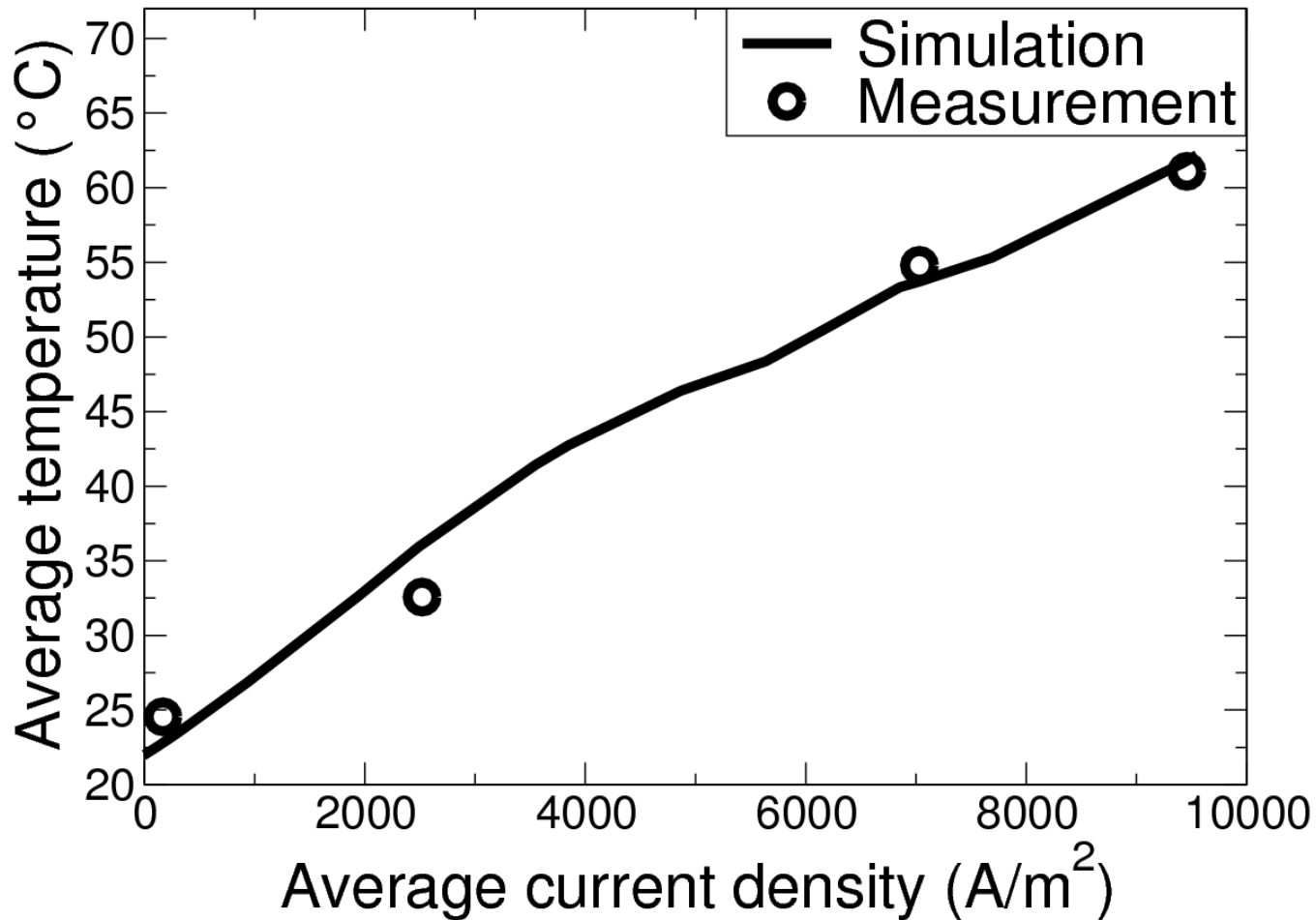
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- Current density prediction very good, predicted temperature gradient too small



Average temperature vs. average current density in reaction layer

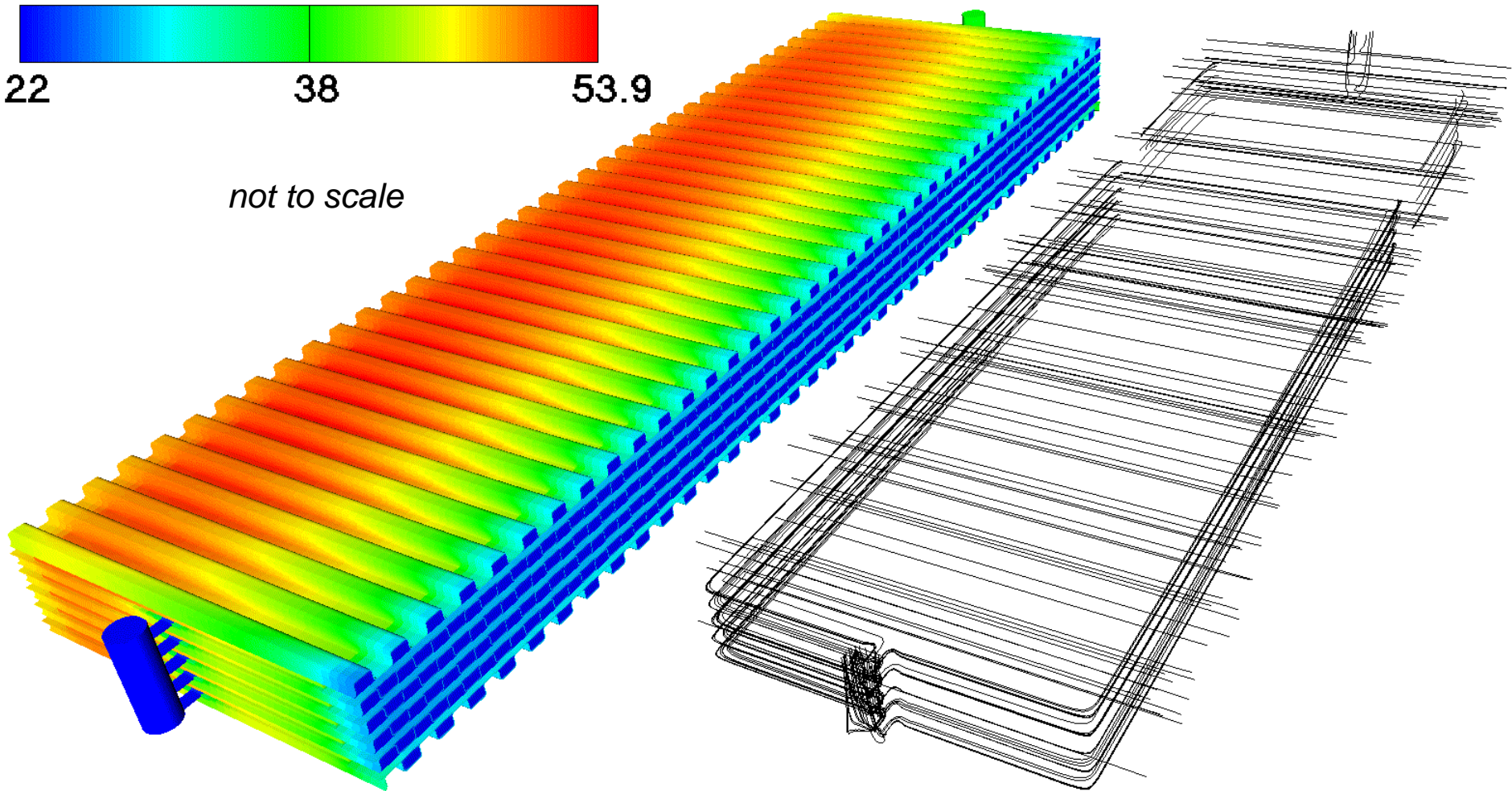




# Simulation of AC64-5 stack – healthy (new) stack



Temperature (°C) and streamlines of whole stack at 0.66 V







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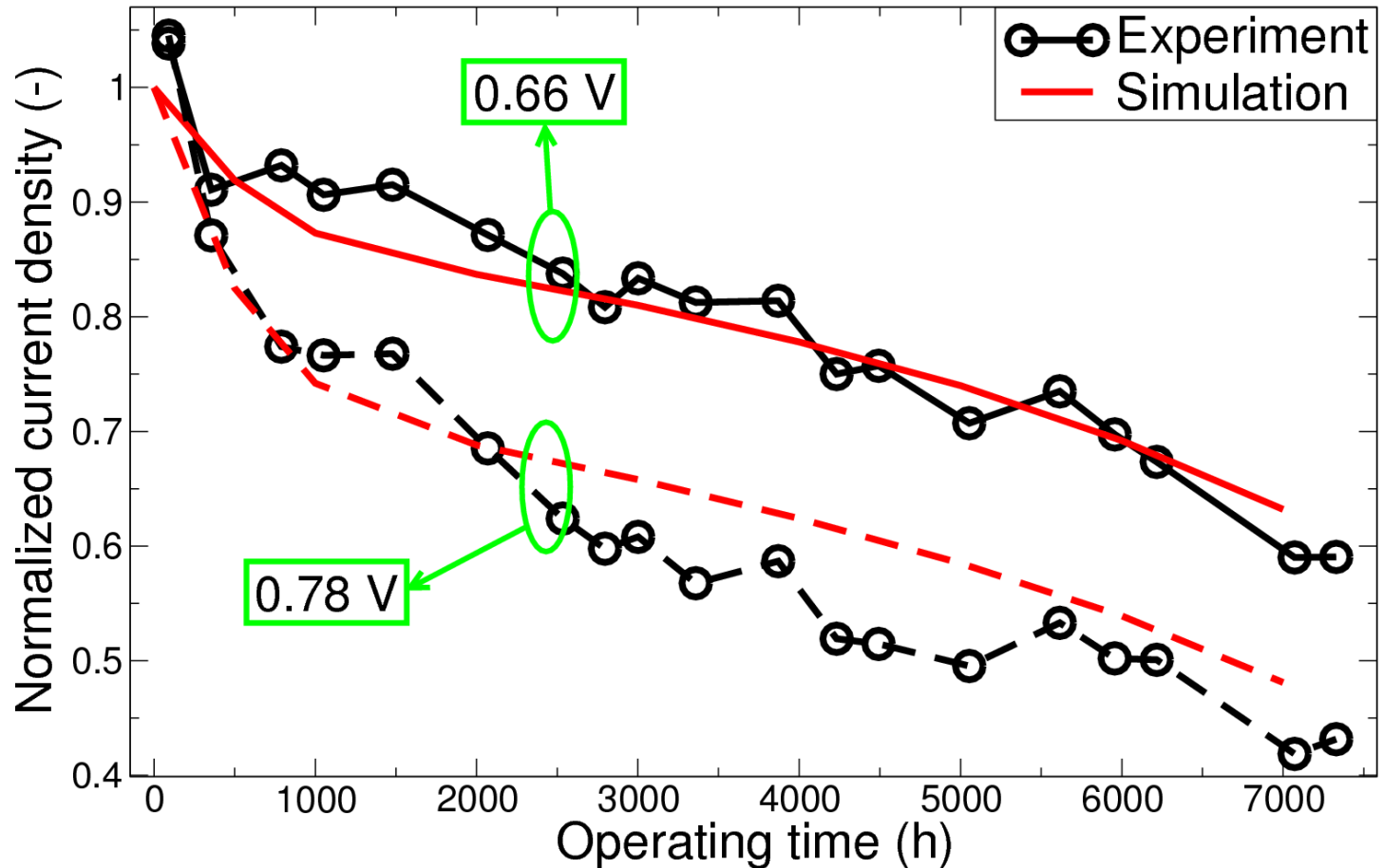
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Comparison between calculated and measured current density drop vs. operating time for two different cell voltages in AC64 stack

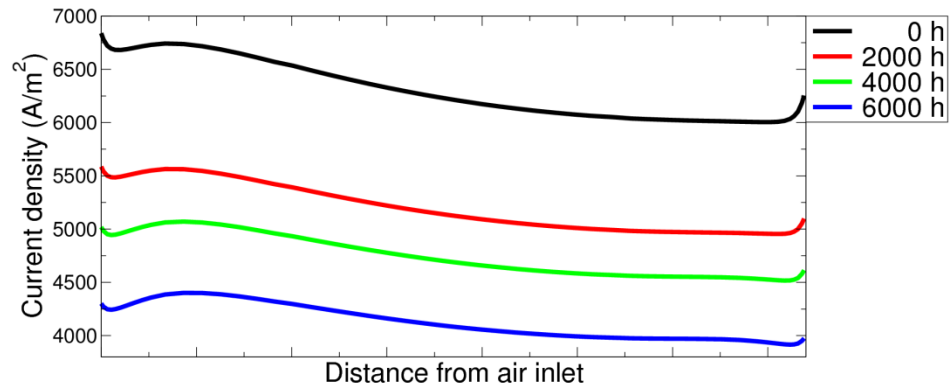
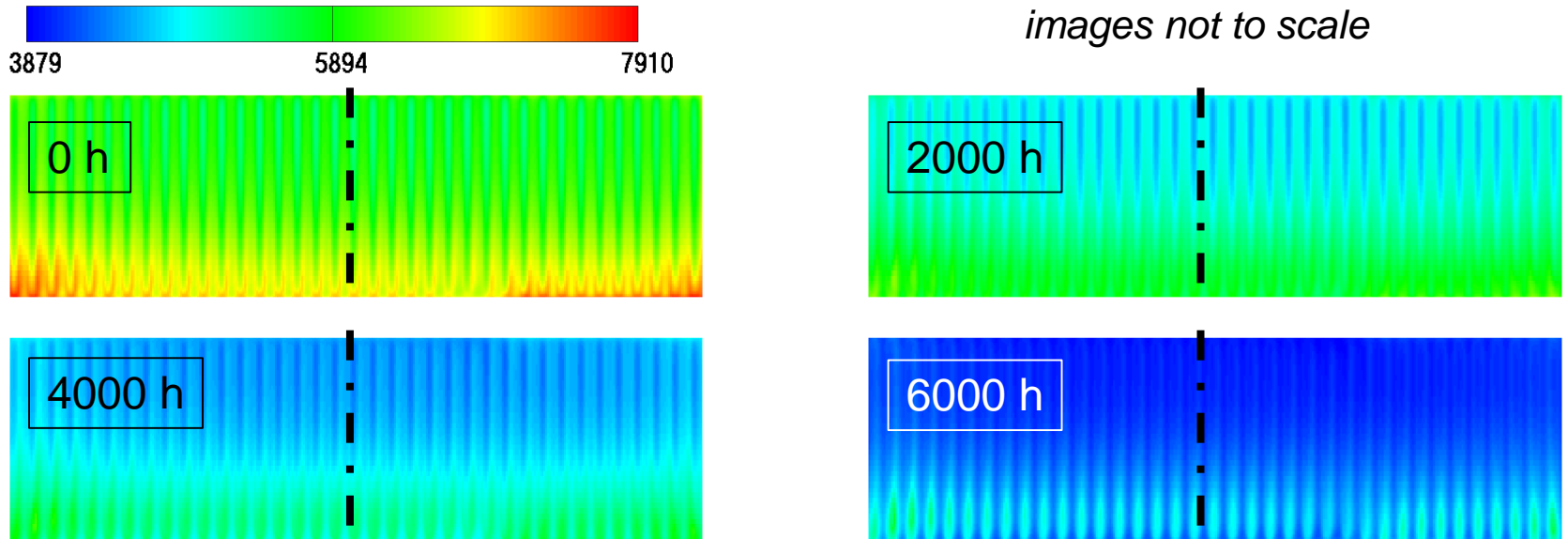




# Simulation of AC64-5 stack – degraded (used) stack



Current density distribution ( $A/m^2$ ) for various operating times at 0.66 V

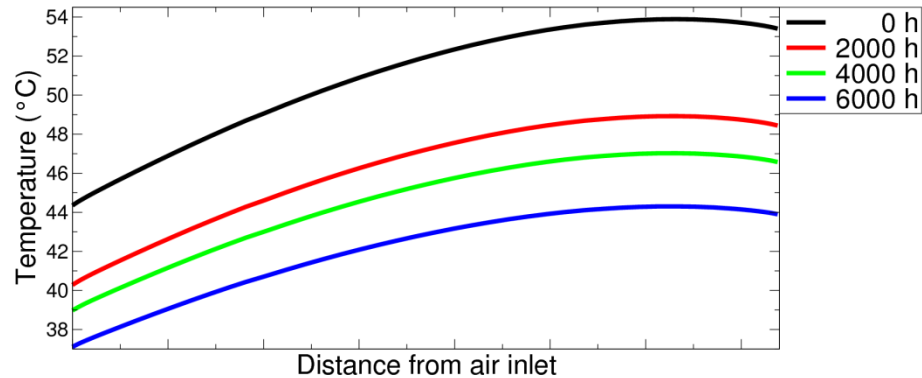
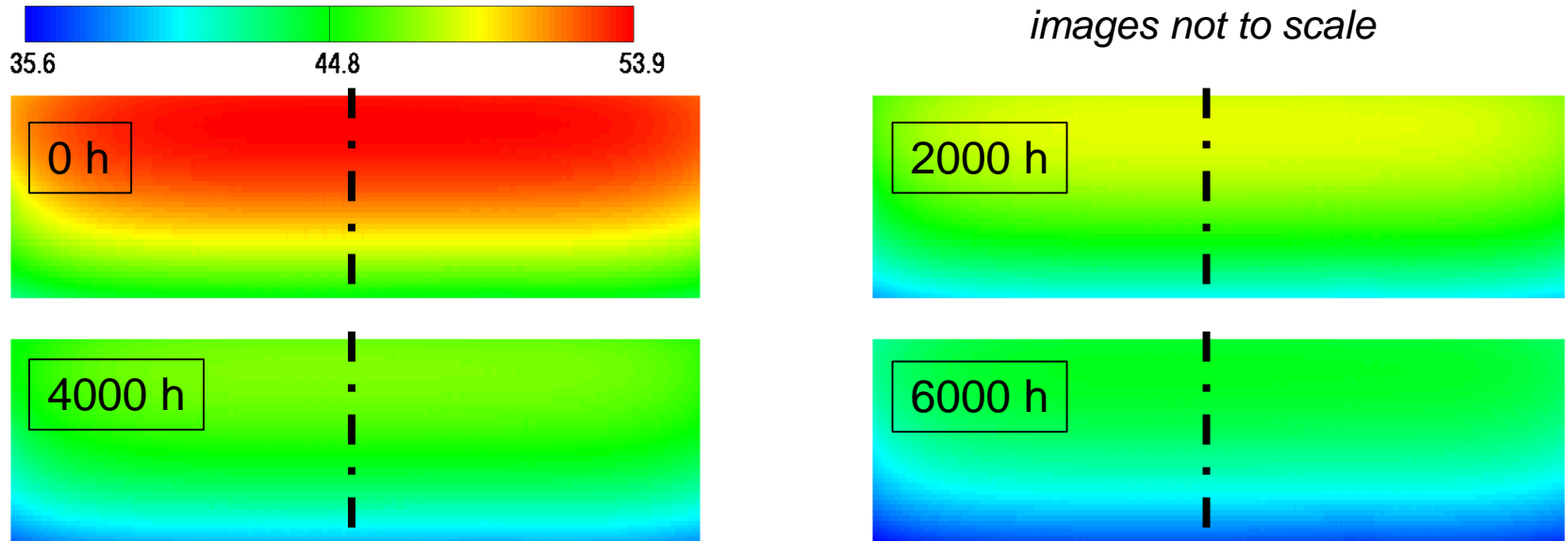




# Simulation of AC64-5 stack – degraded (used) stack



Temperature distribution (°C) for various operating times at 0.66 V





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### Conclusions

- Excellent agreement between simulation and experiment in VI-curve, high frequency losses and average temperature
- Good agreement in current density distribution
- Predicted temperature gradient too small  $\Rightarrow$  further investigations required
- Performance decrease with operating time is predicted with high accuracy

### Outlook

- Extension of catalyst layer model from 0D to 3D
- Implementation of transient effects for PEM fuel cell simulation (load changes, dead end/purge mode)
- Chemically based degradation models for PEM fuel cells

# Thank you for your attention!

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